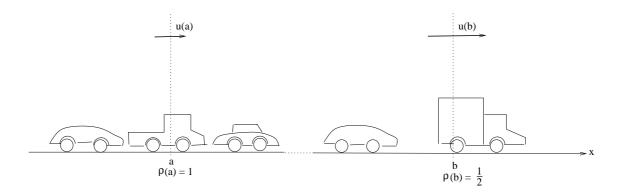
## Chapter 18. Stationary convection - diffusion problems

## The convection problem:

Example: Consider the traffic flow in a highway.



Let  $\rho = \rho(x,t)$  be the density of cars  $(0 \le \rho \le 1)$  and u = u(x,t) the velocity (speed vector) of the cars.

For a highway path (a, b) the difference between the traffic inflow  $u(a)\rho(a)$  at the point x = a and outflow  $u(b)\rho(b)$  at x = b gives the density variation on the interval (a, b):

$$\frac{d}{dt} \int_a^b \rho(x,t) dx = \int_a^b \dot{\rho}(x,t) dx = \rho(a)u(a) - \rho(b)u(b) = -\int_a^b (u\rho)' dx$$

or equivalently

$$\int_{a}^{b} \left( \dot{\rho} + (u\rho)' \right) dx = 0.$$

Now since a and b can be chosen arbitrary, thus we have

$$\dot{\rho} + (u\rho)' = 0$$

Let now  $u = 1 - \rho$ , (motivate this choice), then  $\dot{\rho} + ((1 - \rho)\rho)' = \dot{\rho} + (\rho - \rho^2)' = 0$ , i.e.,

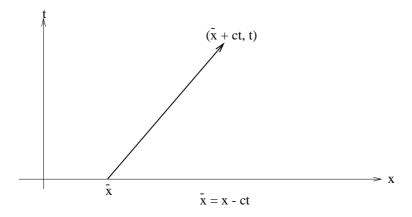
$$\dot{\rho} + (1 - 2\rho)\rho' = 0$$
 (A non-linear convection equation).

Alternatively, we may assume that  $u=c-\varepsilon\cdot(\rho'/\rho),\ c>0,\ \varepsilon>0,$  (motivate). Then we get from (1) that

$$\dot{\rho} + \left( (c - \varepsilon \frac{\rho'}{\rho}) \rho \right)' = 0, \iff \dot{\rho} + c\rho' - \varepsilon \rho'' = 0.$$
 (A convection - diffusion equation).

Which is convection dominated if  $c > \varepsilon$ .

For  $\varepsilon = 0$  the solution is given by the exact transport  $\rho(x, t) = \rho_0(x - ct)$ , because then  $\rho = \text{constant}$  on the (c, 1)-direction.



Note that differentiating  $\rho(x,t) = \rho(\bar{x} + ct, t)$  with respect to t we get

$$\frac{\partial \rho}{\partial x} \cdot \frac{\partial x}{\partial t} + \frac{\partial \rho}{\partial t} = 0, \quad \Longleftrightarrow \quad c\rho' + \dot{\rho} = 0.$$

We rewrite our last convection-diffusion equation for  $\rho$ , by changing the notation from  $\rho$  to u, and replacing c by  $\beta$  and get

$$\underline{\dot{u} + \beta \cdot u' - \varepsilon \cdot u'' = 0}.$$

We compare this equation with the Navier-Stokes equation for incompressible flow:

$$\dot{u} + (\beta \cdot \nabla)u - \varepsilon \Delta u + \nabla P = 0, \quad \wedge \quad \text{div } u = 0,$$

where  $\beta=u,\ u=(u_1,u_2,u_3)$  is the velocity vector, with  $u_1$  representing the mass,  $u_2$  momentum, and  $u_3=$  energy. Further P is the pressure and  $\varepsilon=\frac{1}{Re}$  with Re denoting the Reynold's number.

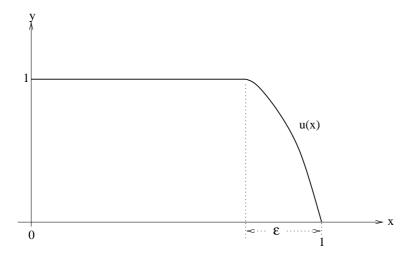
These equations are not easily solvable, for  $\varepsilon > 0$  and *small*, because of difficulties related to boundary layer and turbulence. A typical range for the Reynold's number Re is between  $10^5$  and  $10^7$ .

Example: Consider the

(BVP) 
$$\begin{cases} u' - \varepsilon u'' = 0, & 0 < x < 1 \\ u(0) = 1 & u(1) = 0. \end{cases}$$

The exact solution is given by

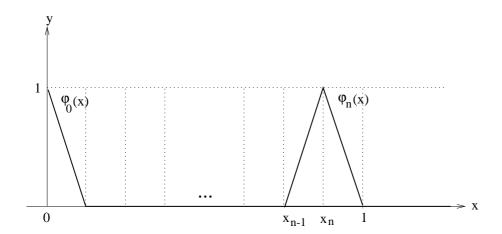
$$u(x) = C\left(e^{1/\varepsilon} - e^{x/\varepsilon}\right), \quad \text{with} \quad C = \frac{1}{e^{1/\varepsilon} - 1}.$$



Note an outflow boundary layer of width  $\sim \varepsilon$ .

<u>FEM.</u> The finite element discretization would be then

$$U(x) = \varphi_0(x) + U_1 \varphi_1(x) + \ldots + U_n \varphi_n(x).$$



The variational formulation:

$$\int_0^1 \left( U' \varphi_j dx + \varepsilon U' \varphi_j' \right) dx = 0, \quad j = 1, 2, \dots n$$

gives the equations

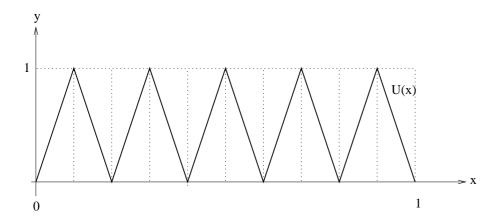
(2) 
$$\frac{1}{2} \left( U_{j+1} - U_{j-1} \right) + \frac{\varepsilon}{h} \left( 2U_j - U_{j-1} - U_{j+1} \right) = 0, \quad j = 1, 2, \dots, n,$$

where  $U_0 = 1$  and  $U_{n+1} = 0$ .

Note that we can also write using "Central -differencing"

$$\underbrace{\frac{U_{j+1}-U_{j-1}}{2h}}_{\text{corresp. to }u'(x_j)} - \varepsilon \underbrace{\frac{U_{j+1}-2U_j+U_{j-1}}{h^2}}_{\text{corresp. to }u''(x_j)} = 0 \quad \Big( \Longleftrightarrow \frac{1}{h} \times \text{the equation}(2) \Big).$$

For  $\varepsilon$  very small this gives that  $U_{j+1} \approx U_{j-1}$ , giving, for even n values, alternating 0 and 1 as the solution values at the nodes:



i.e., oscillations in U are transported "upstreams" making U a "globally bad approximation" of u.

A better method is to approximate  $u'(x_i)$  by an "upwind" derivative:

$$u'(x_j) \approx \frac{U_j - U_{j-1}}{h},$$

which, formally, gives a better stability, however, with low accuracy.

The example itself demonstrates that a high accuracy without stability is indeed useless.

A more systematic method of making FE - solution of the fluid problems stable is through using the:

## Streamline - diffusion method (SDM):

The idea is to choose the test functions of the form  $(v + \frac{1}{2}\beta hv')$ , instead of just v. Then, e.g., for our model problem we obtain the equation  $(\beta \equiv 1)$ 

(3) 
$$\int_0^1 \left[ u'(v + \frac{1}{2}hv') - \varepsilon \cdot u''\left(v + \frac{1}{2}hv'\right) \right] dx = \int_0^1 f\left(v + \frac{1}{2}hv'\right) dx.$$

Here, in the discrete version of the variational formulation, we should interpret the term  $\int_0^1 U''v'dx$  as

$$\sum_{j} \int_{I_{j}} U''v'dx = 0 \text{ (in the case of approximation with piecewise linears)}.$$

Note that  $v = \varphi_j$  implies:

$$\int_0^1 U' \frac{1}{2} h \varphi_j' dx = U_j - \frac{1}{2} U_{j+1} - \frac{1}{2} U_{j-1},$$

which combined with (adding the two)

$$\int_{0}^{1} U' \varphi_{j} dx = \frac{U_{j+1} - U_{j-1}}{2},$$

gives  $(U_j - U_{j-1})$ , which is approximating the first integral in (3) corresponding to the "upwind" scheme.

The SDM can also be interpreted as a sort of least-square method:

Let 
$$A = \frac{d}{dx}$$
 and  $A^t = -\frac{d}{dx}$ ; then  $u$  minimizes  $||w' - f||$  if

$$u' = Au = f \iff A^t Au = A^t f \iff -u'' = -f$$
, the continuous form.

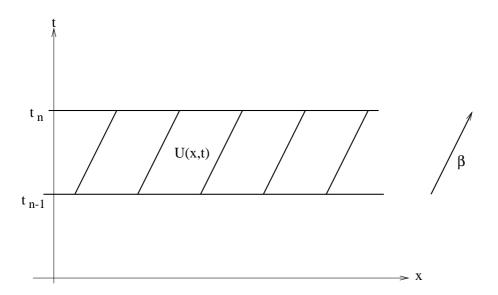
While multiplying u' = Au = f by v and integrating over (0,1) we have

$$\int_0^1 U'v'dx = \int_0^1 fv'dx \quad \text{(Weak form)},$$

where we replaced u' by U'.

For the time-dependent convection problem, the oriented time-space element are used:

$$\dot{u} + \beta u' - \varepsilon u'' = f.$$



Set U(x,t) such that U is piecewise linear in x and piecewise constant in the  $(\beta,1)$ -direction. Combine with SDM and add up some artificial viscosity,  $\hat{\varepsilon}$ , depending on the residual term to get for each time interval  $I_n$ :

$$\int_{I_n} \int_{\Omega} \left[ (\dot{U} + \beta U) \left( v + \frac{\beta}{2} h \dot{v} \right) + \hat{\varepsilon} \ U' v' \right] dx dt = \int_{I_n} \int_{\Omega} f \left( v + \frac{\beta}{2} h v' \right) dx dt. \quad \Box$$